



XYLOOLIGOSACCHARIDES PRODUCTION FROM OIL PALM FROND BY *Trichoderma longibrachiatum* XYLANASE

(Penghasilan Xilooligosakarida daripada Pelepah Kelapa Sawit Menggunakan Xilanase
Trichoderma longibrachiatum)

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Abstract

Oil palm fronds containing rich hemicellulose are low cost resources that could be potentially converted into valuable products such as xylooligosaccharides. The main objective of this study was to investigate the production of xylooligosaccharides from OPF hemicelluloses using *Trichoderma longibrachiatum* xylanase. The OPF hemicellulose extracted by alkaline extraction was hydrolysed by xylanase at pH 4.6, temperature 40 °C, hemicellulose substrate concentration 2 % (w/v) and enzyme concentration 2 U/ml for different period of time from 0 to 48 hours to produce xylooligosaccharides. The hydrolysate obtained from enzymatic hydrolysis was further purified through ultrafiltration using 10 kDa molecular weight cut off membranes. The highest total of xylobiose and xylotriose was found to be 21.91 mg/mL and obtained at 8 hours of hydrolysis time. After ultrafiltration step, xylooligosaccharides mixture were obtained in the permeate and retentate. The highest xylobiose (56.64g/100g) and xylotriose (45.80g/100g) were found in retentate and permeate, respectively.

Keywords: xylooligosaccharides, oil palm frond, ultrafiltration, enzymatic hydrolysis, xylanase

Abstrak

Pelepah kelapa sawit yang kaya dengan hemiselulosa adalah sumber kos rendah yang berpotensi untuk ditukarkan kepada produk bernilai seperti xilooligosakarida. Objektif utama kajian ini adalah untuk menyiasat penghasilan xilooligosakarida daripada hemiselulosa pelepah kelapa sawit menggunakan enzim xilanase *Trichoderma longibrachiatum*. Hemiselulosa yang diekstrak daripada pelepah kelapa sawit menggunakan alkali, dihidrolisis menggunakan enzim xilanase pada pH 4.6, suhu 40 °C, kepekatan hemiselulose 2 % (w/v) dan kepekatan enzim 2U/ml untuk tempoh masa berbeza dari 0 hingga 48 jam untuk menghasilkan xilooligosakarida. Hidrolisat yang diperolehi daripada hidrolisis enzimatik kemudiannya ditulenkan melalui ultrafiltrasi menggunakan membran yang berat molekulnya 10 kDa. Jumlah tertinggi xilobios dan xilotrios adalah 21.91 mg/mL yang diperolehi pada masa hidrolisis 8 jam. Setelah ultrafiltrasi, campuran xilooligosakarida diperolehi dalam 'permeate' dan 'retentate'. Kandungan tertinggi xilobios (56.64g/100g) dan xilotrios (45.80g/100g) ditemui di dalam 'retentate' dan 'permeate'.

Kata kunci: xilooligosakarida, pelepah kelapa sawit, ultrafiltrasi, hidrolisis enzimatik, xilanase

Introduction

Oil palm fronds (OPF) generated the most of waste among the other biomass with 54.17 million tons and 54.24 million tons from oil palm industry in Malaysia for year 2010 and 2011, respectively [1]. The OPF is available daily throughout the year when the palms are pruned during the harvesting of bunches of fresh fruit. It is composed of hemicelluloses, cellulose and lignin. Hemicellulose extracted by alkaline extraction can be used as starting material for xylooligosaccharides (XOs) production. XOs are sugar oligomers made up of xylose unit. XOs can be used as ingredients of functional foods, cosmetics, pharmaceuticals or agricultural products [2]

Enzymatic method is more preferable to produce XOs compared to other methods, because it does not produce undesirable component or high amount of monomers and does not require special equipment [3]. Enzymatic production of xylooligosaccharides performed by xylanase having high endoxylanase and low β -xylosidase activity besides present of others side group enzyme removal include α -arabinofuranosidases, acetylxylan esterase, and α -glucuronidase [4]. Membrane separations, such as ultrafiltration and nanofiltration have been shown to be very promising methods for refining and concentrating several oligosaccharides [3]. Membrane technologies have been applied successfully in conjugation with enzymatic hydrolysis following steam hydrolysis for processing XOs.

Previous study used *Trichoderma viride* xylanase to produce XOs from OPF. However the result showed that the yield of XOs was only 25.64% [5]. Since there is also no purification step was performed in the previous study, thus in the present work, xylanase from *Trichoderma longibrachiatum* was used for enzymatic hydrolysis due to a few reports on their ability to produce high yield of XOs [6-8] following by ultrafiltration step. Therefore, the main objective of this study was to investigate the production of XOs mixture from alkaline extracted oil palm fronds hemicellulose using *Trichoderma longibrachiatum* and ultrafiltration.

Materials and Methods

Raw material

Oil palm frond (OPF) samples used in this study were obtained from local farmers in Perak, Malaysia. The samples were chipped, ground and sieved into fibers with width and length of 0.5 mm and 3 to 8 mm, respectively, and then stored at room temperature prior to use. All chemicals used were of analytical grade unless otherwise stated.

Hemicellulose extraction

Hemicellulose extraction from OPF was conducted according to the method reported by Anis [9] with some modifications. An amount of 50 g sample of oil palm frond chips were soaked in 3 M potassium hydroxide (KOH) with the solid to liquid ratio of 1:10, stirred at 40 °C and 400 rpm with mechanical heat stirrer (HS-30D, WiseStir) for 4 hours. Then, the crude hemicellulose was filtered. The filtrate was acidified with 50 % (v/v) acetic acid to pH 4.8 ± 0.1 and allowed to stand for 24 hours at 4 °C. The extracts were centrifuged (Centrifuged 5702, Eppendorf) at 3500 rpm for 15 min and filtered. The precipitate was washed with 50 mL of 95 % (v/v) ethanol to eliminate acid residue from the sample before dried in an oven (UFB 500, Memmert) at 40 °C for 4 hours. The supernatant was then added with four volumes of 95 % ethanol and was kept for overnight. Hemicellulose in the form of pellet was obtained from precipitate after centrifuged, while the supernatant was discarded. Finally, the pellet was dried in the oven and used as a hemicellulose source.

Enzymatic hydrolysis

A volume of 1 mL of 2 U/mL of xylanase from *T. longibrachiatum* (Sigma, USA) was added to 10 mL of 2 % (w/v) alkaline extracted hemicellulose solution from OPF in 0.05 M citrate buffer at pH 4.6. The mixture was incubated at 40 °C with mild shaking in an incubator shaker (IKA® KS 4000i Control, China). Enzymatic hydrolysis was carried out at pH 4.6, temperature 40 °C, hemicellulose concentration 2 % (w/v) and enzyme concentration 2 U/mL. This hydrolysis was conducted from 0 to 48 hours. Periodically, samples were taken out and the enzymatic reaction was stopped by boiling for 5 min before the samples were subjected to analyses. The hydrolysate obtained at optimal time was further used for purification step using ultrafiltration [10]. XOs contents were determined using HPLC.

Purification of hydrolysate using Ultrafiltration

Purification process was carried out using an Amicon Stirred Ultrafiltration Cell, Model 8400 (Millipore-Amicon, Bedford, MA) pressurized by nitrogen gas. A volume of 50 mL of hydrolysate obtained from hemicellulose

hydrolysis was passed through the ultrafiltration system with 10 kDa molecular weight cut off (MWCO) membrane. The operating condition allowed membrane operating pressure 55 psi at room temperature. The filtration was stopped when approximately 40 mL of permeate was collected. The total sugar in retentate and permeate after ultrafiltration process was determined by phenol/sulfuric acid method. The XO's content was determined by HPLC.

Total sugar analysis

Total sugar content in hydrolysate was measured by using the phenol-sulfuric acid method [11]. An amount of 1 mL of 5 % (w/v) phenol solution and 5 mL of 98 % concentrated sulfuric acid were added to 1 mL of hydrolysate. The mixture was mixed well and kept at room temperature for 10 minutes for color development before being cooled in the water bath (Memmert, Germany) at 25 °C for 20 minutes. The absorbance was measured at wavelength 480 nm by UV spectrophotometer (Perkin Elmer Precise, 35 Lambda, USA). The amount of total sugar was expressed as mg/mL alkaline extracted hemicellulose (pellet).

Monosaccharides determination by HPLC

The content of monosaccharides in the XO's-containing liquor from ultrafiltration process was determined by HPLC (Agilent Technologies 1200 Series, Germany) using Aminex HPX 87P column (300 mm x 7.8 mm). The HPLC was equipped with a refractive index detector (G 1362A, Agilent Technologies 1200 Series, Germany) and column oven (Agilent Technologies 1200 Series, Germany). The sample was filtered through a 0.20 µm nylon syringe filter (Minisart, Sartorius AG, Germany) prior to direct injection into HPLC. The sample was eluted using deionised water as the mobile phase at column temperature of 80 °C and a flow rate of 0.5 mL/min.

Xylooligosaccharides determination by HPLC

XO's were analyzed by HPLC (Agilent Technologies 1200 Series, Germany) equipped with a refractive index detector (G 1362A, Agilent Technologies 1200 Series, Germany), and column oven (Agilent Technologies 1200 Series, Germany). A volume of 2 mL of hydrolysate obtaining from ultrafiltration was filtered through a 0.20 µm nylon syringe filter (Minisart, Sartorius AG, Germany). A 20 µL volume of the filtered sample was injected into HPLC. The sample was eluted using deionised water as the mobile phase. The BioRad-Aminex HPX 42A column (300 mm x 7.8 mm) was used at 80 °C and a flow rate of 0.5 mL/min. Concentration of XO's was measured using an average peak areas compared to the mixture of XO's standards and expressed as mg/mL XO's. Standard calibration curve was plotted based on peak areas against concentration of XO's standards.

Results and Discussion

Monosaccharides Composition of Hemicellulose

The monosaccharide compositions of OPF hemicellulose were xylose, arabinose and glucose. Xylose was the major component with 46.67 % (w/w) found in the OPF hemicellulose indicating the existence of xylan as the main polysaccharides [12], followed by a small amount of arabinose and glucose with 11.01 % (w/w) and 9.01 % (w/w), respectively. Xylose probably originated from the backbone of the hemicellulose [13], while arabinose and glucose came from the side chain [14]. This result is in accordance with the finding reported by Fazilah et al. [15] using similar raw materials.

Enzymatic hydrolysis of OPF

Table 1 shows the enzymatic hydrolysis of OPF for a period of time from 0 to 48 hours using 2 U/mL xylanase concentrations with 2 % (w/v) OPF hemicellulose substrate at pH 4.6 and 40 °C. HPLC analysis indicated that OPF hemicellulose is hydrolysed to xylose and a variety of XO's fractions, which are xylobiose, xylotriose, xylotetraose, xylopentaose and xylohexaose.

During the initial 2 hours, the concentration of xylobiose decreased as much as to 42 % from 7.24 ± 0.44 mg/mL to 4.19 ± 0.06 mg/mL, and the concentration of xylotriose decreased slightly from 8.93 ± 0.16 mg/mL to 8.32 ± 0.47 mg/mL, which corresponds to 7 %. However, the concentration of xylobiose and xylotriose increased rapidly at 8 hours. The highest total of xylobiose and xylotriose was 21.91 mg/mL at hydrolysis time of 8 hours. Further increase in the time from 8 to 24 hours significantly decrease ($p < 0.05$) the xylobiose and xylotriose concentrations.

In the present study, XOs in the range of xylobiose to xylohexaose except xylotetraose were produced by *Trichoderma longibrachiatum* xylanase in all hydrolysis time. This result was in accordance with the study reported by Akpinar et al. [3] for the production of XOs from cotton stalk using *Aspergillus niger* xylanase. The absence of xylotetraose in all hydrolysis time was due to its immediate hydrolysis into smaller oligosaccharides once it was produced. The concentration of xylopentaose increased from 0 to 2 hours, whereas the concentration of xylohexaose increased from 0 to 8 hours. Further increase the hydrolysis time from 8 to 24 hours did not significantly increase the xylopentaose and xylohexaose.

Table 1. Concentration of Xylose and XOs at different time of hydrolysis

Sugars (mg/mL)	Hydrolysis Time (hour)				
	0	2	8	24	48
Xylose	0.04±0.01 ^a	1.74±0.05 ^b	8.46±0.32 ^c	17.78±0.90 ^d	23.79±0.33 ^e
Xylobiose	7.24±0.44 ^c	4.19±0.06 ^b	9.70±0.04 ^d	3.25±0.59 ^a	3.77±0.42 ^b
Xylotriose	8.93±0.16 ^c	8.32±0.47 ^{bc}	12.21±0.59 ^d	0.86±0.67 ^a	7.19±1.12 ^b
Xylotetraose	n.d	n.d	n.d	n.d	n.d
Xylopentaose	3.69±0.13 ^a	9.31±0.11 ^c	6.45±0.51 ^b	5.98±0.25 ^b	5.96±0.11 ^b
Xylohexaose	3.85±0.03 ^a	3.02±0.45 ^a	7.05±0.09 ^b	7.18±0.49 ^b	6.90±0.15 ^b
Xylobiose + Xylotriose (Total)	16.17	12.51	21.91	4.11	10.96

Results are presented as means ± standard deviation (n=3), Mean values followed by different superscript letters in a row are significantly different ($p < 0.05$), n.d: not detected.

Table 1 also shows that extending the reaction time to 48 hours did not significantly increase the production of XOs, but instead produced high amount of xylose. The amount of xylose increased drastically after 2 hours. These results were corroborated with the yield of the XOs, which decreased after 8 hours due to a small amount of XOs was hydrolysed into monosaccharides, thus could also inhibit the production of XOs [16]. The concentration of xylose also increased drastically when the reaction time increased. The concentration of Xylose rose up to 23.79 mg/mL when hydrolysis time increased to 48 hours. The result showed that increasing hydrolysis time resulted in higher xylose production.

Purification of OPF XOs by Ultrafiltration

It can be seen that the composition of permeate with molecular weight of 10 kDa MWCO membrane exhibited higher content of xylotriose, followed by xylopentaose, xylohexaose and xylobiose (Table 2). The xylobiose composition in the initial feed decreased from 27.40 g/100 g to 10.64 g/100 g, whereas xylotriose composition increased from 34.47 g/100 g to 45.80 g/100 g when passing through 10 kDa MWCO membrane. It was found that xylobiose was decreased by 61%, while xylotriose was increased by 33% in the permeate. In addition, xylopentaose and xylohexaose composition in the permeate increased slightly from initial feed with 22 % and 7 %, respectively.

Both xylopentaose and xylohexaose composition decrease in the retentate by 33 % and 38 %, respectively. Other than that, xylobiose composition in the retentate increased significantly ($p < 0.05$) from 27.40 g/100 g to 56.64 g/100 g. This result showed that the composition of xylobiose in the retentate was higher compared to in permeate. However, xylotriose decrease significantly ($p < 0.05$) from 34.47 g/100 g to 18.73 g/100 g in the retentate. The initial feed containing XOs was fractionated with 10 kDa MWCO membrane, clearly showed that the permeate

fraction containing XOs ranging from xylobiose to xylohexaose. In contrast, the retentate fraction containing XOs is ranging from xylobiose to xylohexaose. However, Akpinar et al. [3] found that ultrafiltration with 10 kDa MWCO membrane successfully retained mainly high molecular weight oligosaccharides in the retentate. The presence of low molecular weight oligosaccharides in retentate may be due to fouling mechanism. Fouling mechanism caused by blocking of pore in high cut-off membrane by big molecules, so that transportation of small molecules was hindered. Membrane selection is also very important in order to reduce fouling problem [17].

Table 2. Total sugar concentration and composition of permeate and retentate at 8 hours of hydrolysis.

XOs	Initial feed amount (Total sugar, mg/ml)	Composition of feed (g/100g)	Composition of permeate of MWCO 10 kDa membrane (g/100g)	Composition of retentate of MWCO 10 kDa membrane (g/100g)
Total	35.42	100.00	100.00	100.00
Xylobiose	9.70±0.04	27.40 ^b	10.64 ^a	56.64 ^c
Xylotriose	12.21±0.59	34.47 ^b	45.80 ^c	18.73 ^a
Xylotetraose	0.00	0.00	0.00	0.00
Xylopentaose	6.45±0.51	18.22 ^b	22.23 ^c	12.25 ^a
Xylohexaose	7.05±0.09	19.92 ^b	21.33 ^c	12.38 ^a

Mean ± standard deviation of at least duplicate determinations. Mean values followed by different superscript letters in a row are significantly different ($p < 0.05$).

Conclusion

The highest total of xylobiose and xylotriose was found to be 21.91 mg/mL and obtained at 8 hours of hydrolysis time. After ultrafiltration step, mostly xylooligosaccharides mixture were obtained in the permeate and retentate. The highest xylobiose (56.64 g/100 g) and xylotriose (45.80 g/100 g) were found in retentate and permeate respectively.

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References

- Ofori-Boateng, C. and Lee, K.T. (2013). Response surface optimization of ultrasonic-assisted extraction of carotenoids from oil palm (*Elaeis guineensis* Jacq.) fronds. *Food Science and Nutrition*, 1 (3): 209 – 221.
- Vázquez, M. J., Alonso, J. L., Domínguez, H. and Parajó, P. C. (2000). Xylooligosaccharides: manufacture and application. *Trends in Food Science and Technology*, 11: 387 – 393.
- Akpinar, O., Ak, O., Kavas, A., Bakir, U. and Yilmaz, L. (2007). Enzymatic production of xylooligosaccharides from cotton stalks. *Journal of Agricultural and Food Chemistry*, 55: 5544 – 5551.
- Carvalho, A. F. A., Neto, P. O., Silva, D. F. and Pastore, G. M. (2013). Xylooligosaccharides from lignocellulosic materials: Chemical structure, health benefits and production by chemical and enzymatic hydrolysis. *Food Research International*, 51: 75 - 85.

5. Sabiha-Hanim, S., Nor, M. A. M. and Rosma, A. (2011). Effect of autohydrolysis and enzymatic treatment on oil palm (*Elaeis guineensis* Jacq.) frond fibres for xylose and xylooligosaccharides production. *Bioresource Technology*, 102: 1234 – 1239.
6. Royer, J. C. and Nakas, J. P. (1991). Purification and characterization of two xylanases from *Trichoderma longibrachiatum*. *European Journal of Biochemistry*, 202: 521 – 529.
7. Chen, C. S., Chen, J. L. and Lin, T. Y. (1997). Purification and characterization of a xylanase from *Trichoderma longibrachiatum* for xylooligosaccharide production. *Enzyme and Microbial Technology*, 21: 91 – 96.
8. Akpınar, O. and Bostancı, S. (2009). Xylooligosaccharide production from lignocellulosic wastes with *Trichoderma longibrachiatum* xylanase. *Journal of Food, Agriculture & Environment*, 7 (1): 70 – 74.
9. Anis. M. (2000). Extraction and functional properties of oil palm biomass. Doctoral dissertation, Universiti Sains Malaysia, Penang, Malaysia
10. Akpınar, O., Erdogan, K. and Bostancı, S. (2009). Enzymatic production of xylooligosaccharides from selected agricultural wastes. *Food and Bioproducts Processing*, 87: 145 – 151
11. Dubois, M., Gillies, K. A., Hamilton, J. K., Rebers, P. A. and Smith, F. (1956). Colorimetric method for determination of sugars and related substances. *Analytical Chemistry*, 28(3): 350 – 357.
12. Ruiz, H. A., Cerqueira, M. A., Silva, H. D., Rodríguez-Jasso, R. M., Vicente, A. A. and Teixeira, J. A. (2013). Biorefinery valorization of autohydrolysis wheat straw hemicellulose to be applied in a polymer-blend film. *Carbohydrate Polymers*, 92: 2154 – 2162.
13. Luo, Q., Peng, H., Zhou, M., Lin, D., Ruan, R., & Wan, Y., Zhang, J. and Liu Y. (2012). Alkali extraction and physicochemical characterization of hemicelluloses from young bamboo (*Phyllostachys pubescens* mazel). *Bioresources*, 7(4): 5817 – 5828.
14. Bian, J., Peng, F., Peng, P., Xu, F. and Sun, R-C. (2010). Isolation and fractionation of hemicelluloses by graded ethanol precipitation from *Caragana korshinskii*. *Carbohydrate Research*, 345: 802 – 809.
15. Fazilah, A., Azemi, M. N. M., Karim, A. A., and Norakma, M. N. (2009). Physicochemical properties of hydrothermally treated hemicellulose from oil palm frond. *Journal of Agricultural and Food Chemistry*, 57: 1527 – 1531.
16. Akpınar, O., Gunay, K., Yilmaz, Y., İlevant, O. and Bostancı, S. (2010). Enzymatic process and antioxidant activity of agricultural waste autohydrolysis liquors. *Bioresources*, 5(2): 699 – 711.
17. Gullón, P., González-Muñoz, M. J., Domínguez, H. and Parajó, J. C. (2008). Membrane processing of liquors from *Eucalyptus globulus* autohydrolysis. *Journal of Food Engineering*, 87: 257 – 265.